This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Currently Amended) A process for the treatment of a hydrocarbon charge, at least 80% of the compounds of which have a boiling point which is above or equal to 340°C, in which process:

a) the charge is sent to a fractionation stage during which the recovery takes place of:

- at least one heavy fraction comprising at least 90% by weight of compounds which boil at above 450°C and at below 700°C,
- and at least one light fraction which boils at less than the heavy fraction(s),
- a residuum which boils at more than the heavy fraction(s),

b) at least part of the heavy fraction is sent to an extraction stage during which at least some of the resins contained in said heavy fraction are extracted with a parafinic solvent having 3 to 7 carbon atoms, and a purified fraction is recovered,

c) a mixture is made which comprises at least part of the purified fraction obtained in the extraction stage and at least one light fraction obtained in the fractionation stage, and

d) the mixture thus obtained is sent to a cracking stage.

2. (Original) A process according to Claim 1, in which the content of resins in the 340°C-700°C fraction of the charge is between 3 and 15% by weight.

3. (Previously Presented) A process according to claim 1, in which the heavy fraction resulting from the first fractionation stage comprises a resin content of more than 5% by weight.

4. (Previously Presented) A process according to claim 1, in which at least 20% by weight of the resins contained in the heavy fraction is extracted.

5. (Previously Presented) A process according to claim 1, in which the extraction of the resins of the heavy fraction makes it possible to obtain a purified fraction with a content of polyaromatic compounds comprising up to 5 cycles of less than 2% by weight.

6. (Previously Presented) A process according to claim 1, in which the extraction of the resins of the heavy fraction makes it possible to obtain a purified fraction, the nitrogen content of which is reduced by at least 20% by weight in relation to the heavy fraction which was introduced in the extraction stage.

7. (Previously Presented) A process according to claim 1, in which the extraction stage is carried out in an extraction column, using propane, under the following operating conditions :

- a solvent ratio of between 2/1 and 12/1,
- a temperature at the head of the extractor of between 55 and 95°C,
- a temperature at the bottom of the extractor of between 30 and 80°C,
- a pressure in the extractor of between 300 and 400 MPa, and
- between 2 and 5 theoretical stages.

8. (Previously Presented) A process according to claim 1, in which the cracking stage is hydrocracking.

9. (Original) A process according to Claim 8, in which a residuum fraction is obtained from the hydrocracking stage and is sent, at least in part, to a dewaxing and hydrofinishing section for making oil bases.

10. (Previously Presented) A process according to claim 1, in which a residuum fraction is obtained from the hydrocracking stage and is sent, at least in part, to an FCC unit.

11. (Previously Presented) A process according to claim 8, in which a residuum fraction is

obtained from the hydrocracking stage, and is recycled, at least in part, to the hydrocracking stage.

12. (Previously Presented) A process according to claim 1, in which the cracking stage is catalytic cracking in fluidised bed (FCC).

13. (Original) A process according to Claim 12, in which the FCC stage is preceded by a hydrotreatment stage.

14. (Previously Presented) A process according to claim 1, in which the charge is selected from a direct distillation residuum, a residuum from a conversion process, a coking residuum, a residuum from a hydroconversion process in fixed bed, a residuum from a conversion process in boiling bed, or a mixture of any one of these.

15. (Previously Presented) A process according to claim 1, in which an external charge is added to the heavy fraction entering the extraction stage, said charge being a vacuum distillate or an aromatic extract.

16. (New) A process according to claim 1, wherein the parafinic solvent has 3 to 5 carbon atoms.

17. (New) A process according to claim 1, wherein the paraffinic solvent is a heptane.